

Consideration on
He Resource Conservation for
ILC SRF Cryogenics

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Outline

- Motivation
- Boundary conditions
- An Update suggested: 100% GHe storage, instead of 50/50(%) G-/L- He
- Technical and cost comparisons
- Summary

Motivations to:

- He resource to be 100 % recycled and conserved in the ILC, even in any emergencies and/or power outages more than 3 days.
- Important reasons:
 - No natural He resource in Japan, and
 - It may become a show-stopper for the ILC stable operation, in particular in Japan.
 - We have been experienced with major AC power outages, at least twice: Tohoku Earth Quake (2011), and in an outstanding Typhoon (2019) for more than a week.

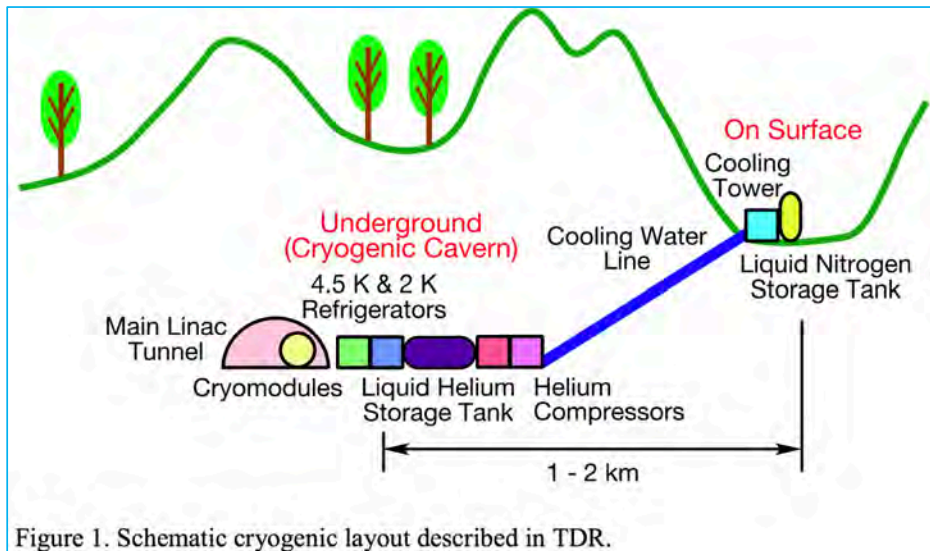
Boundary Conditions

- LHe in the ILC SRF system will entirely evaporate within 3 days after stopping the cryogenics or AC power outage,
- He resource need to be recovered as GHe on surface, within 3 days, in any case, by using emergency recovery compressors operational by using emergency AC power generators.
- The minimum fuel (LNG or Oil) to be reserved on site for this operation. (No more LNG/oil is expected in nation-wide critical situation).

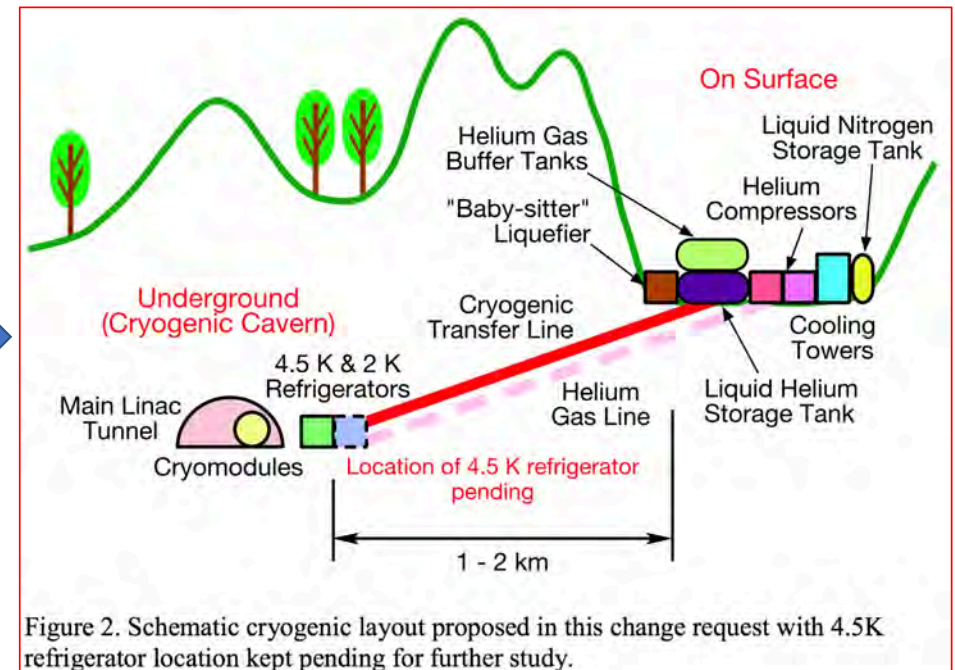
A possible solution

- 100% GHe storage
 - (instead of 50/50(%) LHe/GHe storage)
- Continuous operation of Recovery compressor (20 bar) for > 3days
 - to be supported by Diesel/emergency AC power generators.
- 12 (3x4), 20-bar GHe tank is required
 - (instead of 6 GHe tank + 1 LHe dewar + Liquifier)

ILC Cryogenics Layout-Design Updated in 2017 -- Change Request 09 (CR-09)

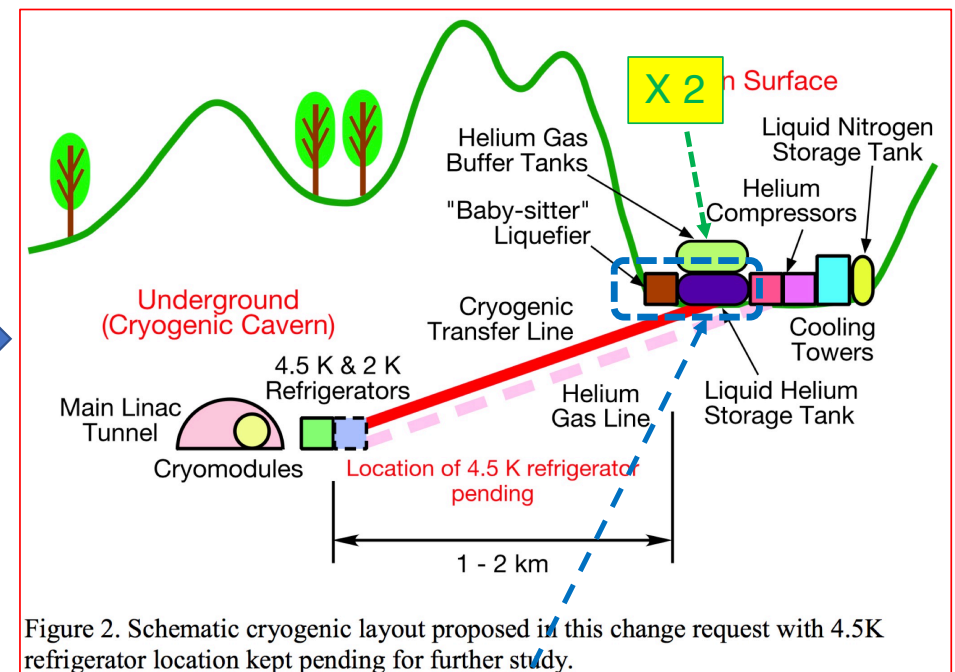
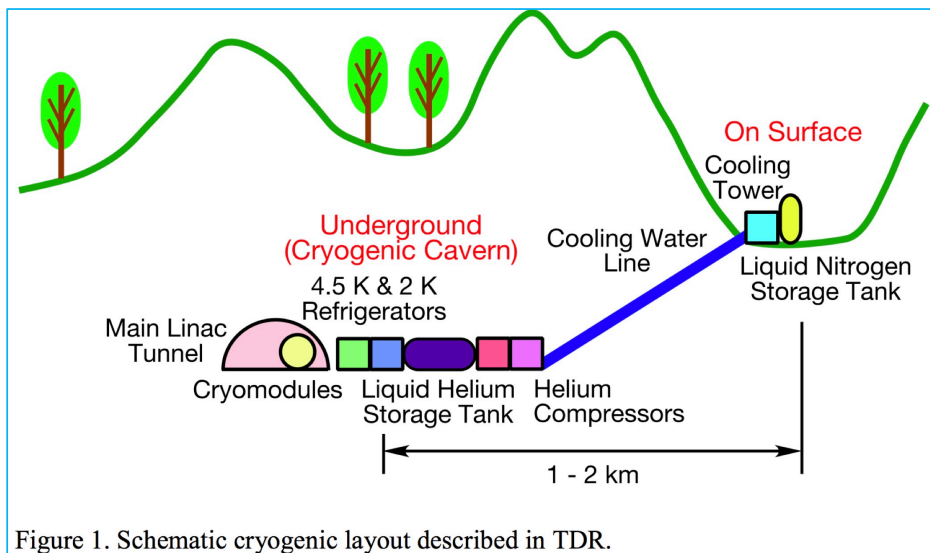


TDR



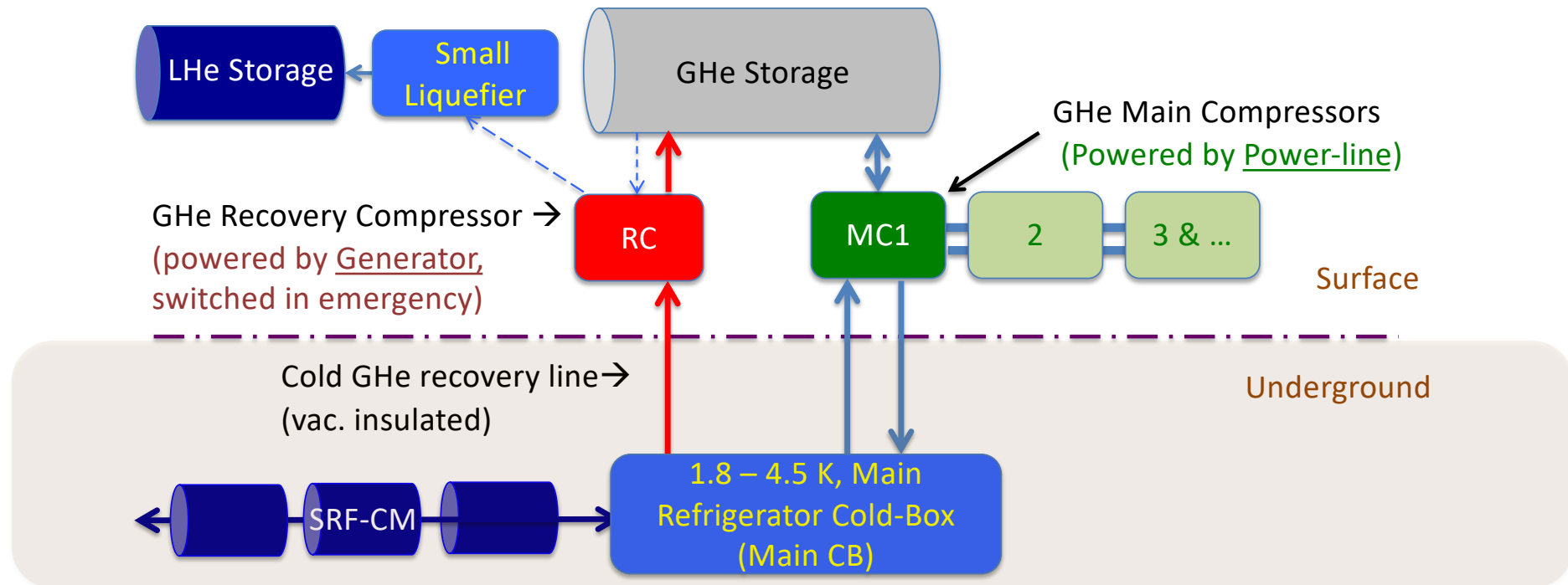
CR-09

ILC Cryogenics Layout-Design Updated in 2017 -- Change Request 09 (CR-09)



Today, we will discuss the **emergency operation**: to be simplified by **doubling GHe Buffer Tanks**, and eliminating a small (Baby-Sitter) He Liquefier and a LHe storage tank (reservoir) /

He Flow Lines in Emergency to Recovery



Operation Sequence in emergency to resume steady state modes (under investigation):

1. GHe recovery using RC (powered by Generator for < 24 hrs, (electric capacity: < 1 MW / plant
 2. Recovery of MC1 (and 2, 3, ...) and Main CB, for LHe to be kept in CM after power-recovery
 3. LHe to be produced in LHe storage for a period of 5 ~ 7 days, by using RC powered by power line
- (Note: Balance of LHe and GHe storage capacity to be further investigated and globally discussed)

A design-update studied in 2017

ML Cryogenics

T.Okamura, H.Nakai, A.Yamamoto

KEK

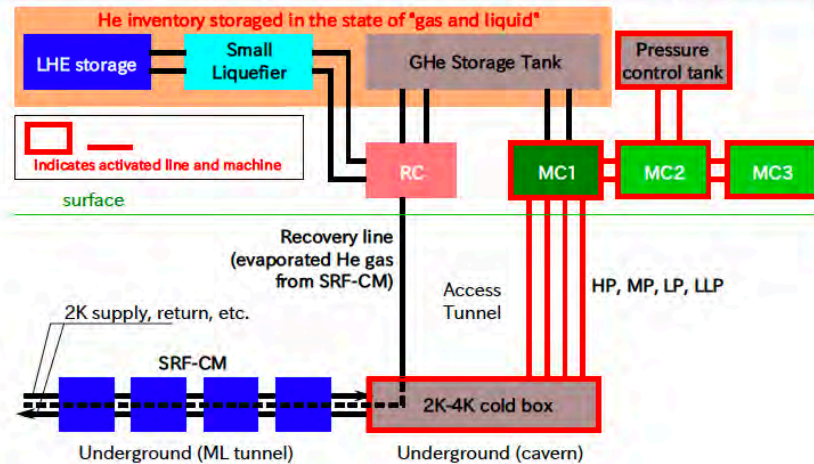
2017/3/13

Contents

- ① Flow and TS diagram
- ② Inventory
- ③ Diagram for power failure etc..
 - Necessity equipment for power failure and other operation modes
- ④ Mass flow requirement during power failure
- ⑤ Buffer tank and small liquifier system
- ⑥ Discussion about inventory storage scheme
 - Cost evaluation
 - Required exclusive area
- ⑦ Summary

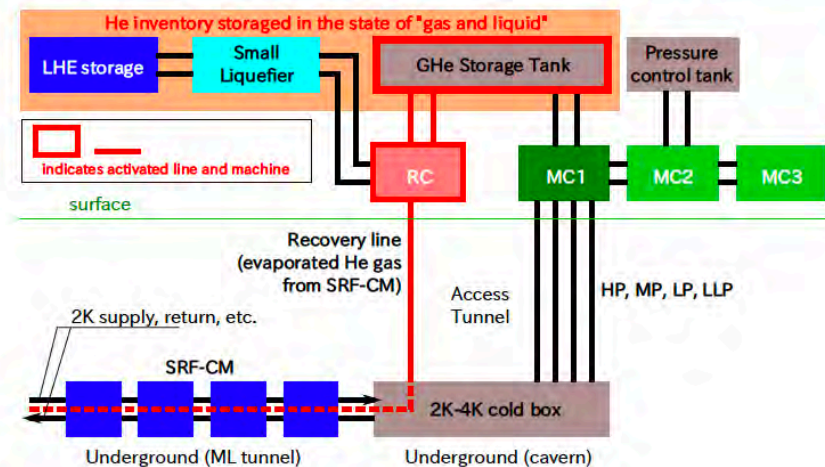
ILC SRF Cryogenics Operation Modes

Block Diagram (during Steady State Operation)



- LHE storage is almost empty during steady-state mode.
- During steady state operation, maintenance of small liquefier should be done.

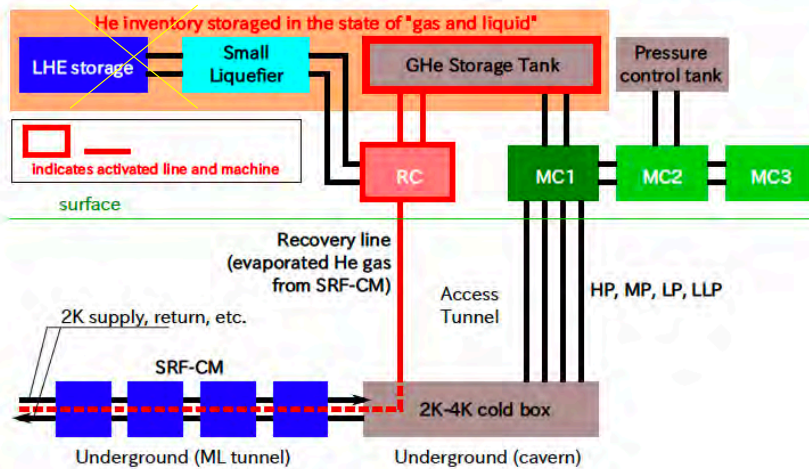
Block Diagram (during Power Failure Operation)



- RC is operated by using Natural gas/oil generator.
- Other equipment keeps halting condition

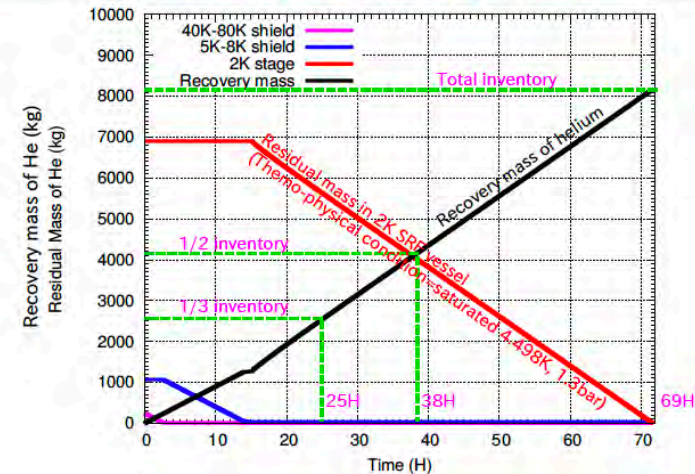
ILC SRF Cryogenics Operation Modes

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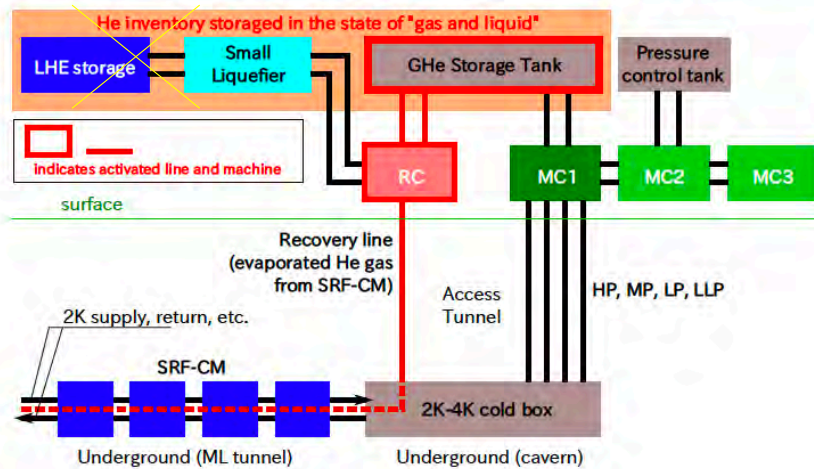
Results (2): Recovery Mass



- Mass flow rate of boil off gas can be reduced to around 30 g/sec.
- 1.5 days to recover half inventory into the 6 buffer tanks/plant.
- 3.0 days to recover all inventory into 12 buffer tanks/plant.

ILC SRF Cryogenics Operation Modes

Block Diagram (during Power Failure Operation)



- RC is operated by using Natural gas/oil generator.
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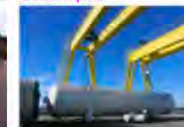
How to set up buffer tanks

- 6 buffer tanks / plant. \Rightarrow 12 tanks / location.
- Transportation and unloading scheme should be considered carefully.

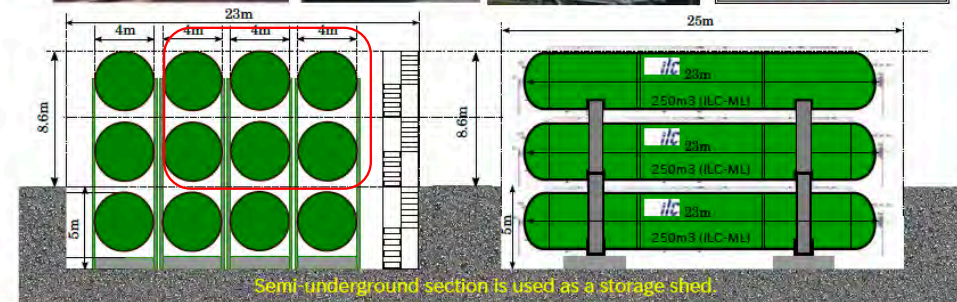
6 buffer tanks (each for 250m³)
example of JT60SA (NAKA / Japan)



Unloading of 250m³ tank
at NAKA port



250m³ buffer tank
Weight = 70t
H=4.3m (including base)
W=4m, L=23m



Comparison Item		12 buffer tanks scheme	6 buffer tanks and LHE Dewar scheme
Cryo components for recovery system	buffer tanks	12	6
	recovery compressor	400kW	400kW
	small liquefier	-	280L/h
	LHE dewar	-	42000L
	cryogenic pipe	-	4 cryo pipes (3-5m)
	cryo control system	-	necessary
Piping through access tunnel	HP	318.5mm	318.5mm
	MP	508mm	508mm
	LP	406mm	406mm
	LLP	406mm	406mm
	Recovery line	165.2mm	165.2mm
exclusive area on surface(m2)		1265	1265
necessity for building		-	necessary
Cost	buffer tanks	6.72	3.36
	recovery compressor	0.7	0.7
	Cold box	-	4.4
	LHE dewar	-	1
	Transportation	1.8	0.9
	unloading crane	0.4	0.4
	Site construction	1.2	0.6
	SUM	10.82	11.36

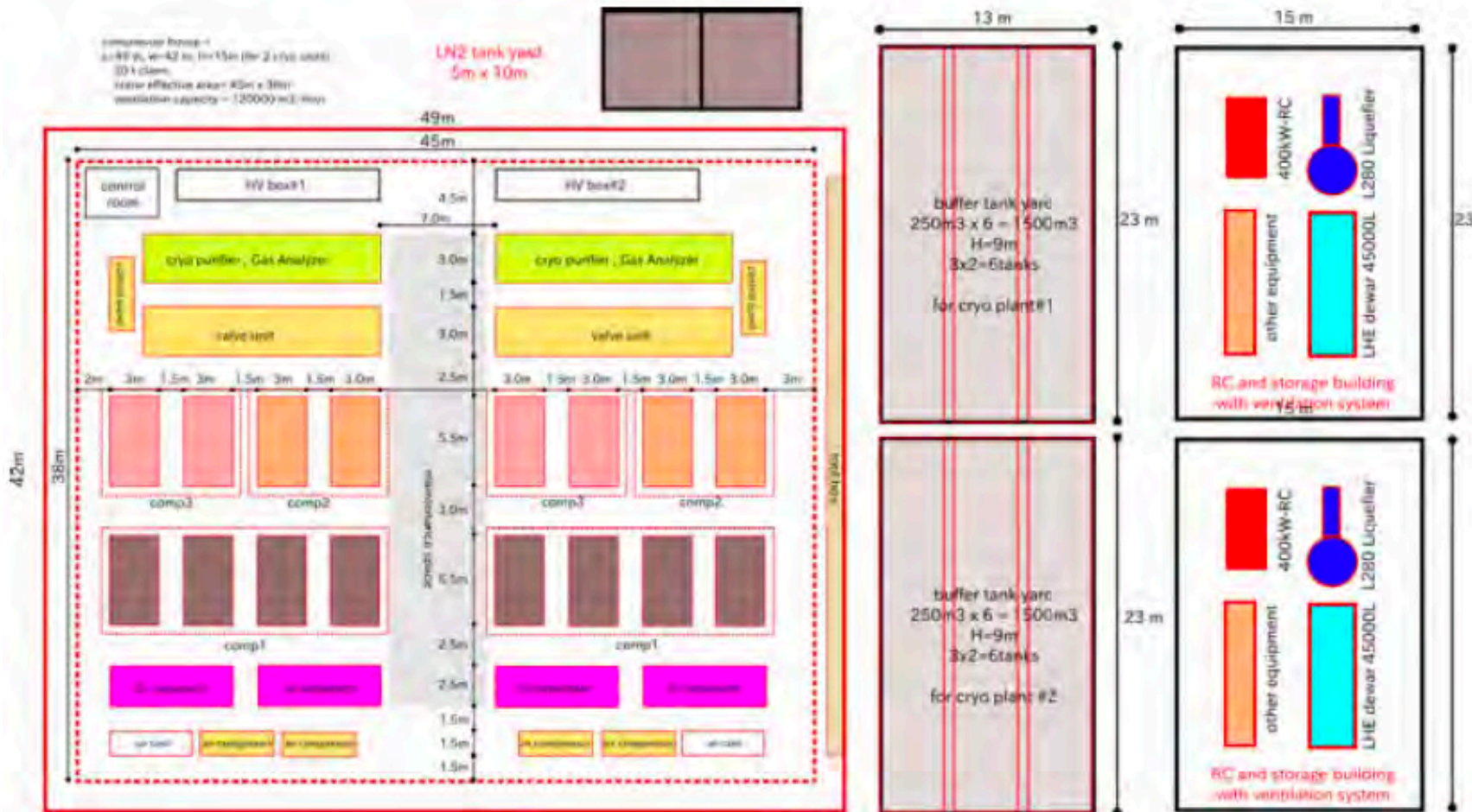
Comparison Item		12 buffer tanks scheme	6 buffer tanks and LHe Dewar scheme		
buffer tanks		12	6		
Recovery time		1 week	3 days		
Manufacturing cost		10.82	11.36		
Required surface area		1263	1265		
SUM		10.82	11.36		

- Recovery time can be reduced from 1 week to 3 days in the case of GHe storage scheme.
- Manufacturing cost without small liquefaction system is a little bit cheaper than half and half mixing storage scheme.
- Required surface area is almost same each other. (if config. shown P19 is applied)

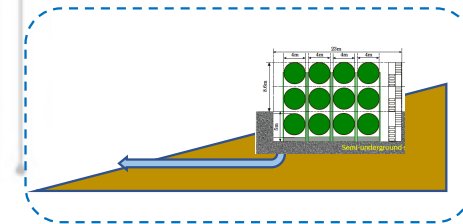
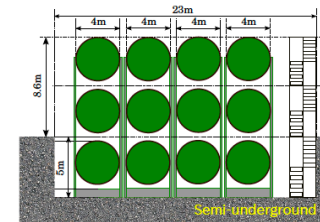
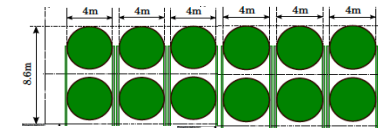
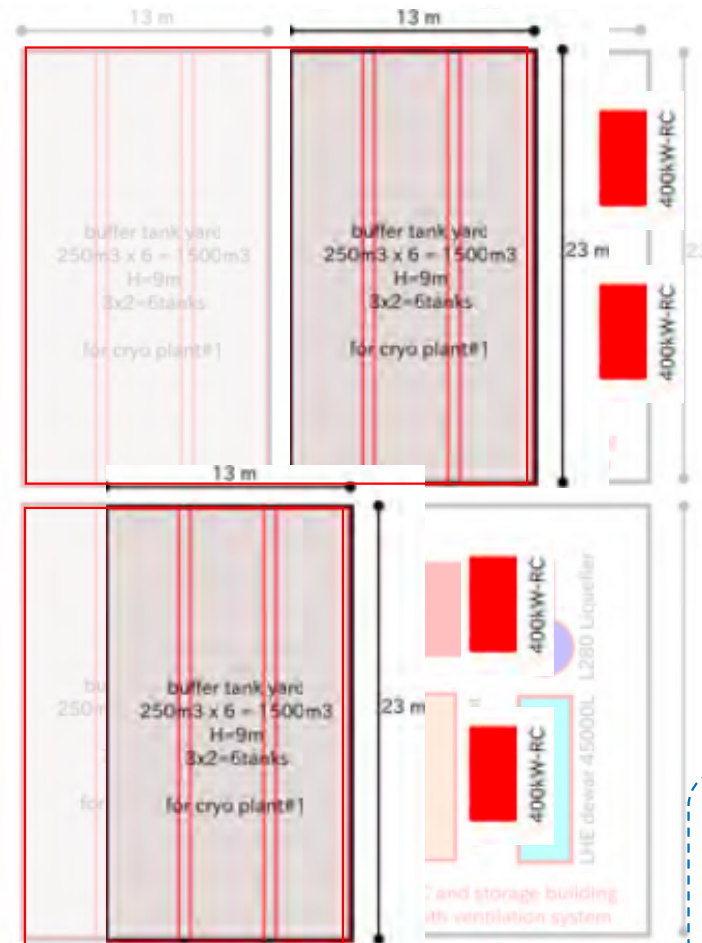
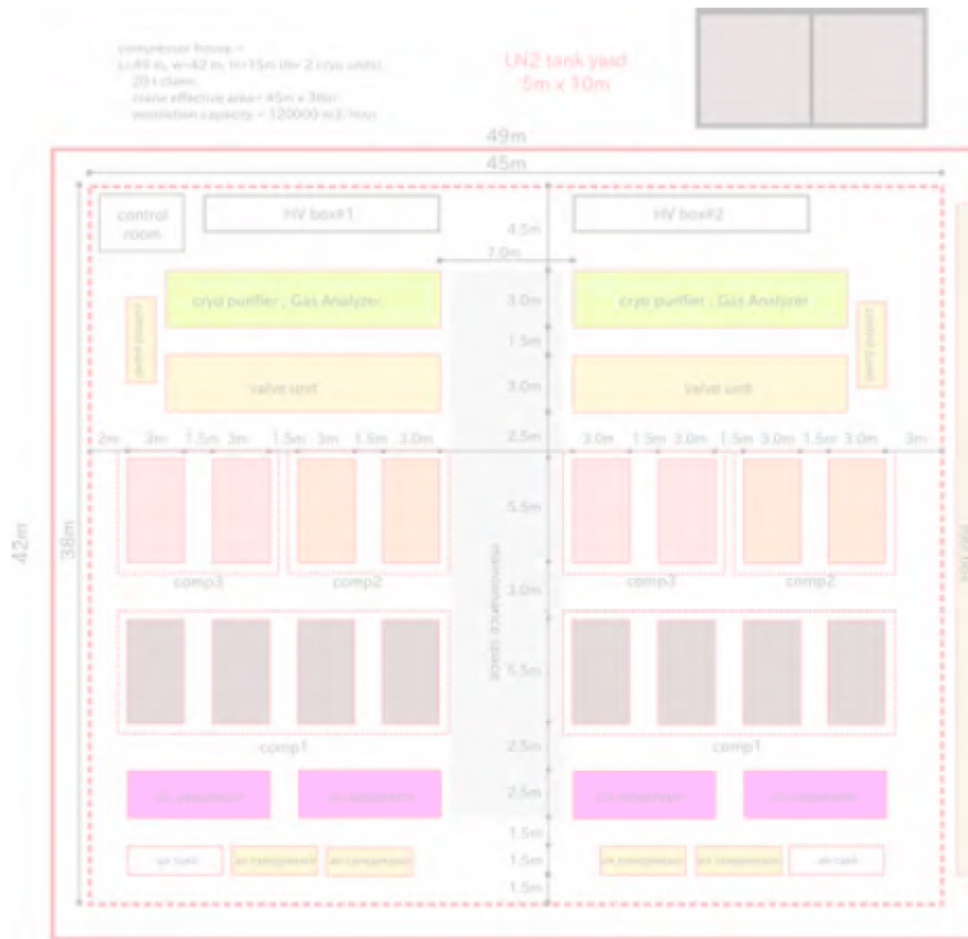
Storage Scheme unit : (**)		buffer tank	Small liquefaction system	Other, Transport etc.	Total Cost
12 buffer tanks	w/o small liquefier	6.72	0	4.1	10.82
6 buffer tanks	w/ small liquefier	3.36	5.4	2.6	11.36

Storage Scheme unit : (m2)		buffer tank	Small liquefaction system	Other, Transport etc.	Total Area
12 buffer tanks	w/o small liquefier	46m x 25m	8m x 14m (RC)		1263
6 buffer tanks	w/ small liquefier	23m x 25m	30m x 23m (RC, Liquefier, LHe dewar)		1265

Surface Layout for 2 plants



Surface Layout for 2 plants



Summary (1)

Power Failure

- Instead of Storage Scheme introduced in TDR, not only LHE dewar but also GHE buffer tanks are employed for preventing loss of He inventory during power failure.
- Recovery compressor (RC) should be located on surface but its capacity should be enough small to be operated using LNG generator during the failure. Several hundreds kW can be acceptable. (MW order can not be acceptable.)
- To perform this, recovery mass flow rate during the failure should be reduced. Enthalpy recovery operation seems effective way to reduce the mass flow rate.
- According to the simulation based on toy model, mass flow rate can be reduced to around 30 g/sec. In this case, if 6 tanks with 250 m³ are located on surface, resting state of MCS and MCB for 1.5 days can be acceptable.

The design change already authorized by TCMB

Comparisons of CR-09 and the Update proposed

	CR-09	Update proposed
# GHe Buffer Tank	6 (3 x 2 layers)	12 (4 x 3 layers)
Small He Liquefier	Needed	Not needed
LHe Storage Tank (Reservoir)	Needed	Not needed
Surface area required Lowered base than GL	Baseline Not needed	Equivalent or smaller Needed (~ 3 m)
Emergency Operation:		
He recovery time: --> emergency AC power required	7 days (2 x 3 + alpha)	3 days
Periodic operation during shut-down	Require for baby-sitting	Not required
Redundancy for emergency. required	RCs and He liquefier	RCs only
Cost	Baseline	Equivalent or lower

A Design-Update Proposal:

- Simplify the He recovery system:
 - Doubling numbers of GHe storage tank (6 --> 12)
 - Eliminating {small He Liquifier + LHe storage/reservoir}
 - Except for specific location such as a main plant at each e- and e+ linac site for overall backup
He reserve: 20 ~25 % for the whole He resource amount, for long term stability and risk management.
 - It may be wise to reinforce the redundancy for the Recovery Compressors (RCs) with an additional backup RC.
- The above design-update may realized much simpler emergency operation with well predicted and limited emergency AC power source.
- No cost-increase is expected, and a minor cost-saving may be expected.

Reserved

Summary (2)

Maintenance and other operation

- When all inventory is recovered for maintenance season, small liquefier is needed. RC can also be applied to small liquefaction system.
- Fraction between Liquid and Gas can be optimized by considering site environmental condition.
 - Recently, we considered 1/2 in Gas and 1/2 in LHE.
 - to be discussed further with Tohoku group.
- Recovery time for the total inventory is within 1 week by using small liquefaction system. To perform this, MCS and MCB have to be operated continuously during recovery mode.
- Tentative stop of the Small liquefaction system such as planned outage can be acceptable. To ensure it, allowable pressure should be 10 bar or so and less heat load into the dewar such as 0.2-0.5 %/day should be used.

Do not need to be concerned, In case of doubling GHe tanks

Evaporated mass vs Buffer tank volume

Recovery Time and Buffer tank volume are shown at around 30 g/sec.

HE Inventory		evaporated mass flow (kg/sec)	recovery time		Number of 250m3 Buffer tank	
(kg / plant)			(H)	(Days)	required	contingency
40K shield	246	0.03	2	0.1		
5K shield	1068	0.03	10	0.4		
2K SRF	6901	0.03353	57	2.4		
1/3 inventory	2738	0.03	25	1.1	4	2
1/2 inventory	4108	0.03	38	1.6	6	2
Total inventory	8215	0.03291	69	2.9	11	2

Time to fill up at 30 g/sec.

- 4+2=6 tanks (1/3 inventory) \Rightarrow 25H
- 6+2=8 tanks (1/2 inventory) \Rightarrow 38H
- 11 tanks (total inventory) \Rightarrow 69H

Further detailed dynamic simulation will be performed continuously instead of using TOY model.